

Biofuels from coastal deserts: the sustainability case for a Salicornia bigelovii-based biorefinery

Ayah Alassali, Tolutola Oyetunde, Khalid Rashid, Jorge Rodríguez, Jens Schmidt and Mette H. Thomsen (e-mail: <u>aalassali@masdar.ac.ae</u>, <u>toyetude@masdar.ac.ae</u>, <u>krashid@masdar.ac.ae</u>, <u>irodriguez@masdar.ac.ae</u>, <u>jschmidt@masdar.ac.ae</u>, <u>mthomsen@masdar.ac.ae</u>).

Chemical and Environmental Engineering Program, Masdar Institute of Science and Technology, PO Box 54224, Abu Dhabi, United Arab Emirates.



Thursday, December 19, 2013

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Masdar Institute

The Masdar Institute of Science and Technology (Masdar Institute) is a graduate level, research-oriented university which is focused on alternative energy, sustainability, and the environment.

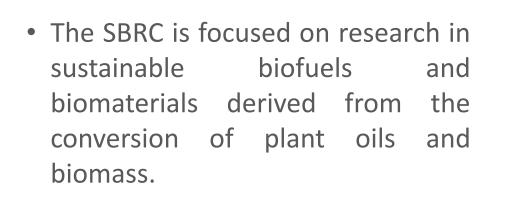


SBRC

Masdar 5



 The Sustainable Bioenergy Research Consortium was established by the Masdar Institute of Science and Technology.









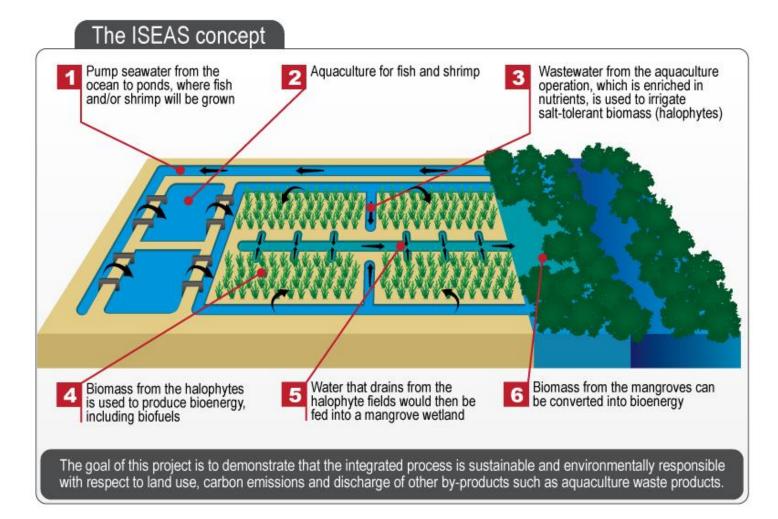
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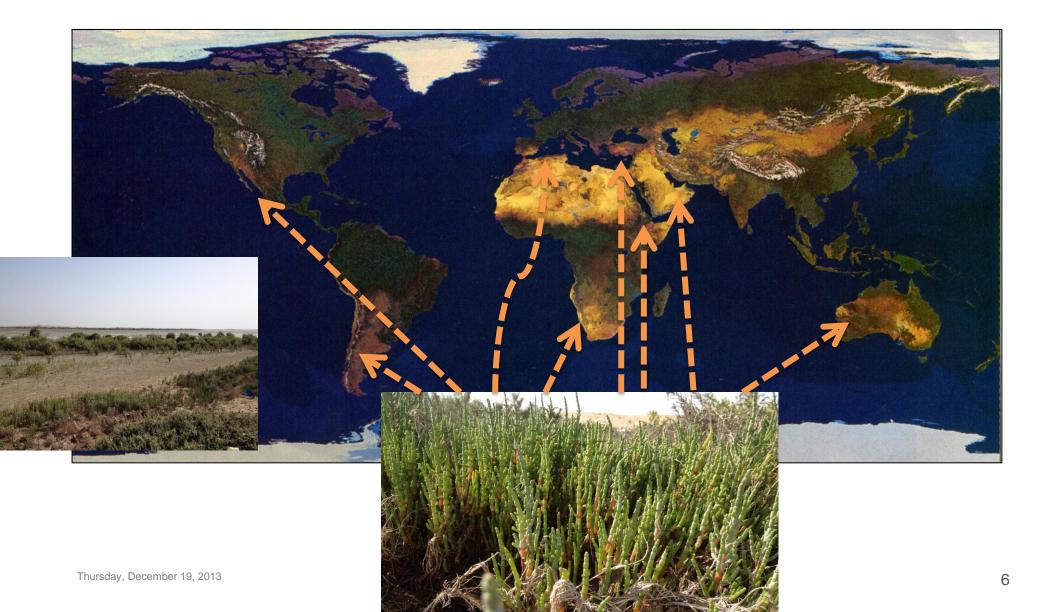


Introduction

ISEA







Feedstock



Feedstock: Salicornia bigelovii

- Salt-tolerant oil crop
- Can grow on every continent, excluding Antarctica





Composition Data

Table 1. Salicornia straw waste chemical composition before and after being washed, as experimentally obtained (Chaturvedi, 2013)

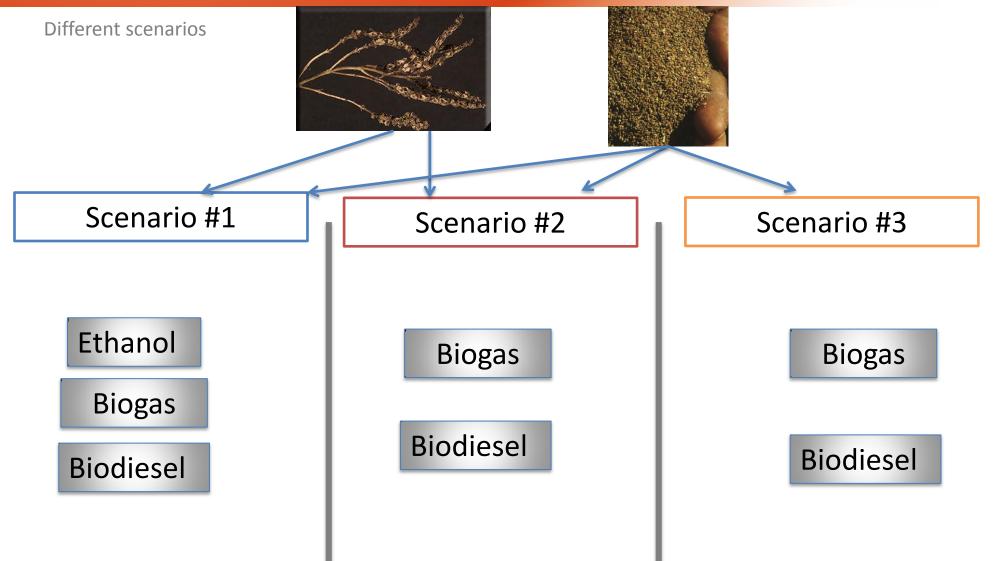
Components	% of Dry Weight, before washing	% of Dry Weight, after washing
Glucan	10.15	25.79
Xylan	7.95	21.57
Arabinan	6.93	5.73
Klason lignin	5.82	7.69
Structural ash	6.8	5.51

- Oil represents 28% of the seeds
- Protein represents 31.2% of the seeds

Chaturvedi, T. (2013). Evaluation of Bioenergy Production from Lignocellulosic Biomass of Salicornia Bigelovii. Masdar Institute, UAE.

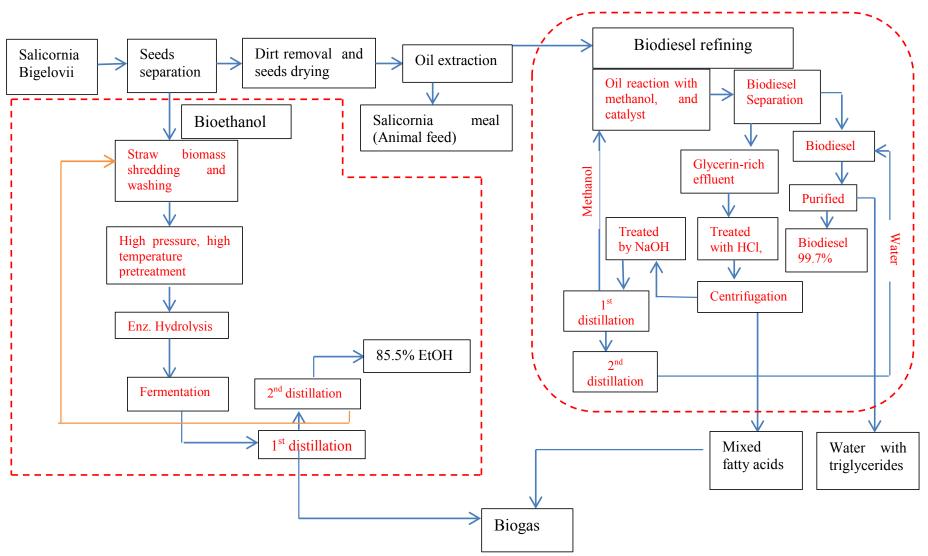
Methodology







Scenario #1



Methodology



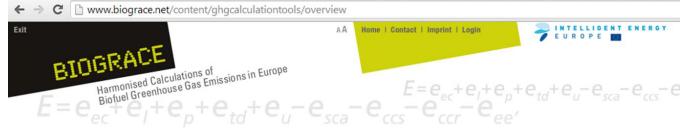
SuperPro[®] Designer Handling and Preparation Section **Oil Extraction Section** P47/SC-101 **Biodiesel Production Section** Generic Box P-46/P118 P40/SL-101 P-38/CSP-101 P-50 / SDR-101 Solids Storage Seed Separation P-51 / GBIG-103 Rm P-53 / GBX-104 Spray Drying Seed Preparation Oil Extraction(with Hexane) P-45 / HX-109 Salicomia Meal Cooling HCI P-20/106/102 P-4/TNK-101 P-44/GBX-101 Maing S-130 Methanol storage tank Vacuum System 1 S-143 P-30 / HX-16o 🦕 📲 Raturned Water S-14 P-29/H0(-16) P31/P-111 Vake-up10-1 P-37/V-104 Purp Heating Heating VELASH P-26 / DC-104 P-57 / BC-101 Belt Conveying P21/V-102 P-5/THK-102 P-13/R-101 P-14/DC-101 P-58 / SR-101 Mixing Vessel Catalyst storage tank P-16 / R-10 S-126 Reactor P-19/DC-102 Centrifugation Shredding Reactor P-60/WSH-102 Centrifucation Washing (Bulk Row) -AHPSies **BioEthanol Production Section** Process Steam ₽17/P-107 P36 /P-114 Salicomia OI Storage Tank Pump S-121 Pump P-24/DC-108 P-27 / P-11 Centrifucatio P-32 / C-101 P-18/V-101 MEOH DISTLL P-61 / R-103 Mixing Vessel Pretreatment P-65 / R-104 Enzymatic Hydrolysis S-129 P-34/C-10 P-22/P-108 P-25 / V-103 +Yeast H20 DISTILL Pump Mixing Vessel P35/P-113 P-41 / TNK-106 P-70 / MOE-108 P-69 / V-110 Рлтр Storage Vaing Storage S-184 P216/C-104 Distillation **Biogas Production Section** P-63 / FR-101 Production Fermentors Biogas 3.14 MT/h P-71/GBX-102 P-72/V-105 P-21a / C-103 P-1/MX-105 Anaerobic Digestors Storage Distillation Mixing BioEthano P-75/V-107

EIOH Storage (7-day Capacity)



Life Cycle Assessment (LCA)

- Greenhouse Gas emission (GHG) and Energy Return On Investment (EROI) were subjects of analysis and evaluation throughout this study.
- Data for energy content and CO_{2eq} emission of the materials, utilities and energy sources used in our process were based on values obtained from SuperPro[®] combined with harmonized calculations of biofuel GHG in Europe; attained from the European Commission protocol (Annex V of the Renewable Energy Directive 2009/28/EC).





Item/equipment	Notes/values	
Process	Continuous process, 330 working days	
Total land area	5000 ha	
Biomass yield (Kg/ha/yr)	16247.00 (<u>Russel W. Stratton, 2010</u>).	
Seeds production (gseeds/Kg total	122 (<u>Russel W. Stratton, 2010</u>).	
mass)		
Salicornia bigelovii	Ranged from 0.01\$/kg to 0.05406\$/kg	
Capital equipment cost	costs were based on the model published by the joint bioenergy institute.	
Hexane-extraction plant capital cost	Based on rapes' seeds plant	

Russel W. Stratton, H. M. W., James I. Hileman. (2010). Life Cycle Greenhouse Gas Efrom Alternative Jet Fuels Project 28: Massachusetts Institute of Technology.

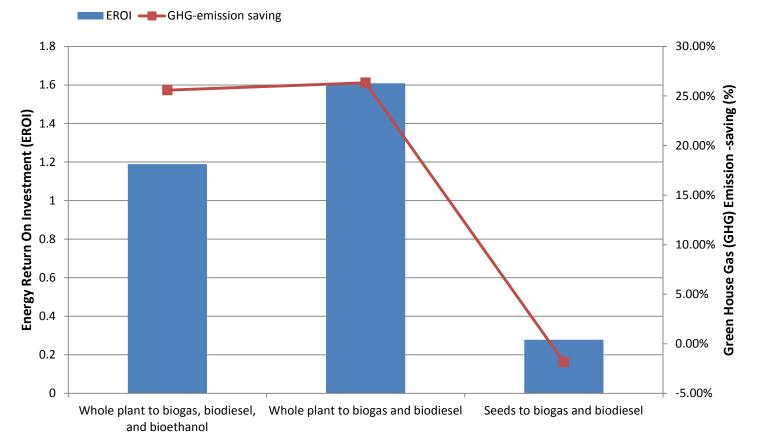


Economic and material results

Economic Parameters			
	Scenario 1	Scenario 2	Scenario3
	(Whole biomass to Biodiesel, bioethanol and biogas)	(Whole biomass to Biogas and Biodiesel)	(Seeds nly to Biodiesel and Biogas)
	0,	0 /	U <i>Y</i>
Total Investment (\$)	45,659,000.00	39,300,000.00	24,943,000.00
Total Revenues (\$/yr)	36,730,000.00	27,131,000.00	8,149,000.00
Operating Cost (\$/yr)	31,536,000.00	18,298,000.00	9,565,000.00
Gross Margin (%)	17.3%	36.4%	-17.4%
Payback Period (Year)	4.3	2.9	26.6
IRR before Taxes (%)	25.55	46.48	-

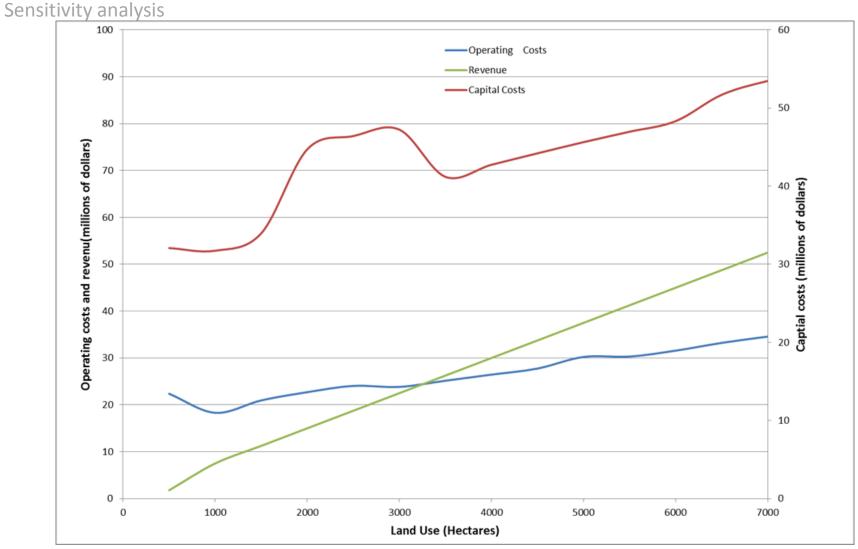


EROI and GHG results



EROI and GHG emission savings for the three different scenarios

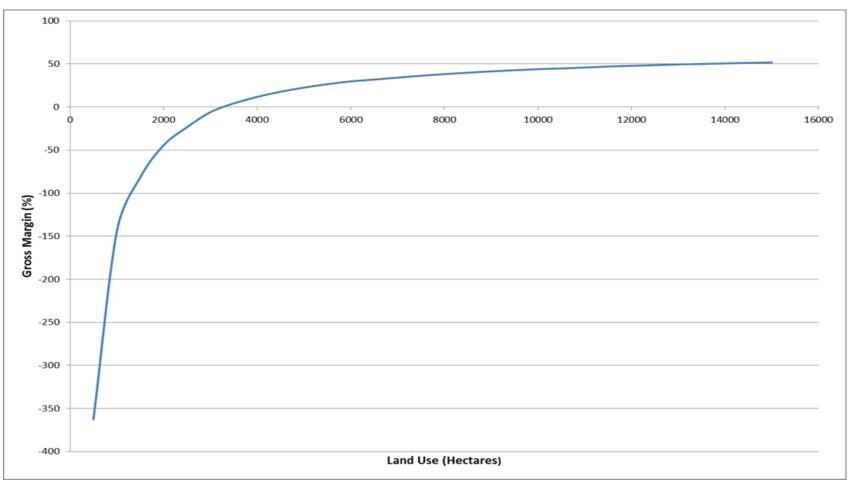




Thursday, December 19, 2013 Variation of costs with land cultivated



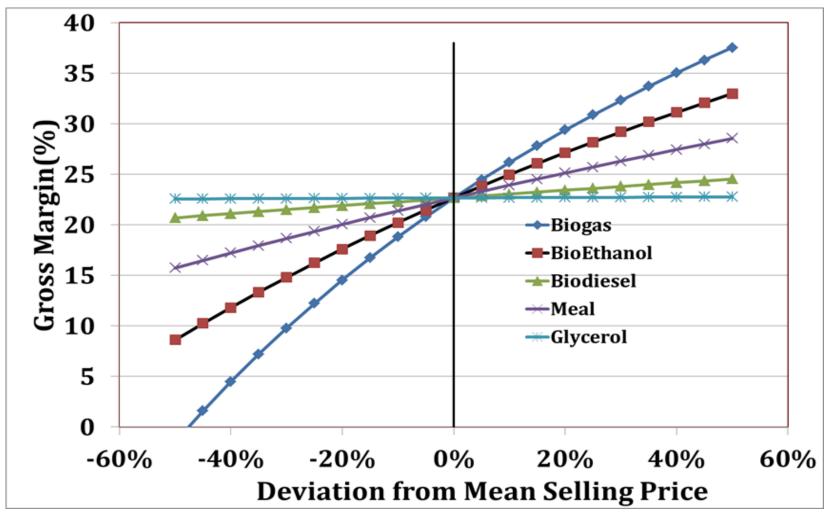
Sensitivity analysis



Variation of Gross margin with land cultivated



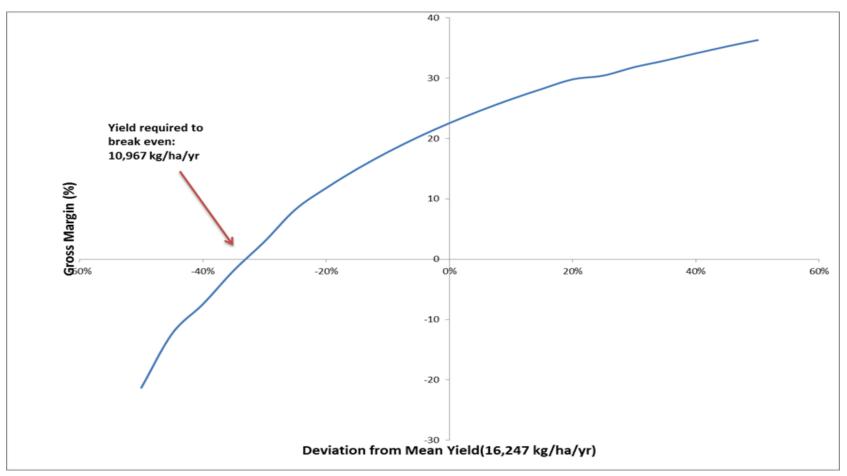
Sensitivity analysis



Effect of selling prices on biorefinery profitability



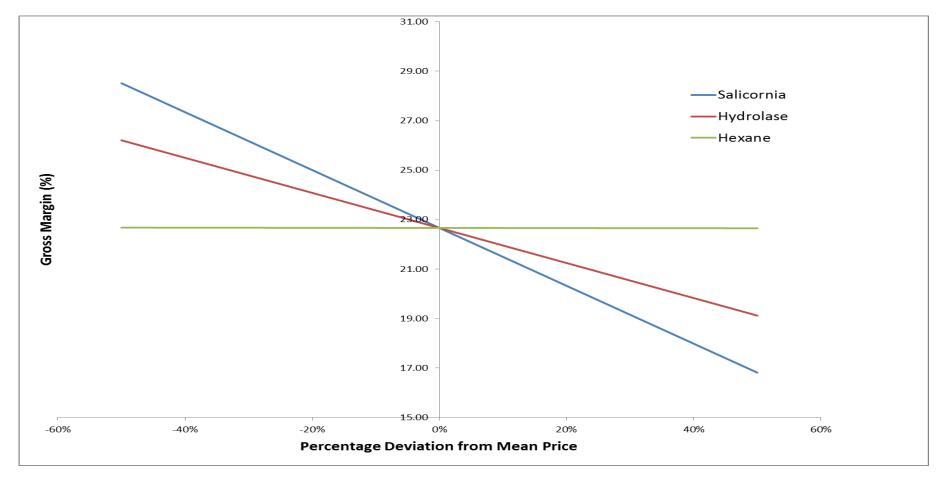
Sensitivity analysis



Effect of Salicornia yield on process profitability (based on 5,000 hectare farm)



Sensitivity analysis



Effect of some cost prices on biorefinery profitability



- A Salicornia-based biorefinery is both economically feasible and environmentally sustainable.
- Salicornia-based biorefinery showed comparable EROI values to first generation-based biorefineries, despite the energy intensive pre-treatment processes involved.
- It is critical to optimize the bioethanol process (reducing capital and operating costs) in order to minimize the economic risk associated running a biorefinery with biogas as the main product.



Thank You

Ayah Alassali aalassali@masdar.ac.ae